Indicator	Key information
Vapour Load	$V_{\text{bottom}} = (R+1)D - (1-q)F$
Energy Demand	$V_{ m top} = (R+1)D$ $L_{ m top} = RD$ $Q_{ m condenser,total} = V_{ m top}\Delta H_{ m top}^{vap}$ $Q_{ m condenser,partial} = L_{ m top}\Delta H_{ m top}^{vap}$ $Q_{ m reboiler,total} = (V_{ m bottom} + B)\Delta H_{ m bottom}^{vap}$ $Q_{ m reboilerpartial} = V_{ m bottom}\Delta H_{ m bottom}^{vap}$
Operating Cost	$\dot{M}_{ m phase} = rac{Q}{\Delta H^{vap}}$ $\dot{M}_{ m sensible} = rac{Q}{C_p \Delta T}$ $\dot{W}_{ m pump} = rac{F M_{w,F} g \Delta h_p}{\eta}$
Capital Cost	Cost of distillation column Cost of heat exchangers Cost of pumps Cost of pipework and control
Total Annualised Cost	Total capital cost adjusted per year of project life Operating costs